# Manufacturing of Polymer Packaging

# ■ 2.1 Extrusion of Resins

The first step in making polymer packaging is to melt the thermoplastic resins and then form them into films or sheets or into an end product like a cap, bottle, or cup. The machines with which this is done are called extruders. An extruder has two main components, a barrel and a screw. Both are made of alloy steel and are very robustly constructed because a pressure of several hundred bars arises during melting. The resins are furnished sometimes with additives that are abrasive; the extruder must be able to work such a product without getting damaged. Besides hard alloy steel, the inside of a barrel and the screw are treated through a series of physical processes like heating and quenching in water to produce high hardness. Whereas the barrel is a plain pipe, the screw is constructed in a very complicated manner. Around a shaft, helical threads are cut with different channel depths. The barrel has a number of heaters and the same number of fans on the outside. The heaters heat the barrel from the outside, and the fans cool it when necessary. Generally, the extruders for melting resins have one screw, a so-called single screw extruder (SSE). If a resin mixture is to be melted where mixing is very tough, then a twin screw extruder is used. The additive manufacturers have such twin screw extruders. The manufacturers of general packaging materials like film, sheet, and tube use single screw extruders. An extruder has three functions: convey the resin, melt it completely, and homogenize the melt, which is then processed into the target material.

An extruder is described according to "Euromap" with three numbers, for example, 1-25-30. The first number stands for the number of screws, the second one the length of the extruder in terms of its cylinder diameter (D), and the third figure is the diameter in millimeters. It is usual to describe the different lengths of different parts of an extruder in terms of its diameter. So the length of the conveying zone in a 25 D may be 10 D, the compression zone 7 D, and the homogenizing zone 8 D. Generally, the extruders have a length of 20 to 30 D, depending upon what parts are integrated into the screw. For thermally stable polymers like PE or PP, a longer

extruder can be used because the resin can be kept hot longer without any material damage. For PVC or PVdC, which are very unstable under heat, the length of an extruder is less.

### 2.1.1 Technology of Extrusion

As already mentioned, the functions of an extruder are to convey, melt, and homogenize a resin before purging.

The screw has a solid shaft of constant or increasing diameter toward its end. Helical flights divide the screw in pitches. The screw has generally three zones (Fig. 2.1). In the first zone, the channel volume in the pitches is constant, and hence the resin is simply conveyed in this zone. In the second zone, the channel volume is reduced by reducing the channel depth, so the resin is compressed here. At the same time, the barrel is heated from the outside, and the resin melts completely. In the third zone, the metering zone, the channel volume is again constant so the melt can be mixed and homogenized properly to keep a constant temperature and viscosity. High-quality packaging materials can only be manufactured if the melt is free from specks (unmolten resin) or dirt particles and is homogeneous. At the end of most extruders, an adapter is placed to create a certain back pressure, so the melt stays a bit longer in the extruder to get better homogenized in the metering zone. The applied back pressure depends upon the resin type and is generally 50 to 100 bar. A film from an inhomogeneous melt shows streaks, which arise through inhomogeneous refraction of light through the film.

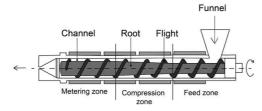


Figure 2.1 Standard three-zone extruder

### Standard Three-Zone Extruder

Although only one end of the heavy screw is mounted with the gear system or directly with the motor and the other end is free, it does not rub the barrel during rotating. The melt inside the extruder stabilizes the screw position. Once mounted, the extruder is fed with a resin, and it is always kept full with melt, even if it is

turned off. During restarting the barrel is heated until all of the resin melts, and it can then turn. To accelerate the process, the extruder is always fed with a so-called cleaning resin, which is a low-melting resin type, before stopping production. When restarting an extruder, a lot of melt is always lost, until all of the parameters are optimum for the next production. To avoid the loss of material and time, extruders generally run around the clock.

Important facts in producing an ideal melt for a packaging application are an extruder with the proper screw, the choice of the proper resin, the proper additive packet, and finally the proper working parameters. In particular, it is very important to not overheat the extruder. If the extruder is overheated, then resin may burn and produce brown to black particles. Some of them stick to the barrel inner wall. Even if later, good melt quality is produced, the burned particles leave the barrel wall from time to time, which leads to a dirty melt. Spots or even holes in the films or pipes are produced. It may take a whole day to clean the extruder.

The extruder is mounted on a robust base. The screw is turned by a powerful electromotor via a suitable gear system to achieve different RPMs for the screw. The resin is poured into the extruder through a funnel at the beginning of the extruder. To avoid premature melting of the resin, the barrel is cooled at this position. Premature melting of the resin may jam the extruder and then no resin can be fed.

The nozzle of the extruder is connected with subsequent tools to produce the desired material, for example, an annular ring for blown film, a coat hanger die for chill roll films, or injection-molding tools.

### Types and Technology of Different Screw Types

A typical screw is shown in Fig. 2.2. The drive shank is mounted on the gear or directly on the motor. It has helical flights and three sections, the feed, compression, and metering sections. The channel depth in the feed section is high and reduces gradually at the compression section as simultaneously the root diameter increases. The resin melts through heat from friction and from external heat supplied outside the barrel. Lastly, the melt is homogenized in the metering section before it is purged out. The pitch is constant throughout the screw. Compression is also possible by reducing the pitch rather than reducing the channel depth. The leading edge of the flight pushes the resin and melt forward. Both pressure and friction are high in this section. The trailing edge has, in contrast, no pressure function. The screw tip can have different forms, depending on use. The screw is the main part of an extruder because through proper construction it is possible to process a particular resin in a particular way. First it must fulfill the proper compression that is necessary to melt the resin. The screw may have a constant shaft diameter and reducing pitch length at the compression zone, or the shaft could have an increasing gradient with the pitch length constant.

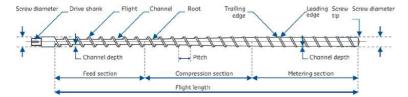


Figure 2.2 Standard three-zone extruder screw, courtesy of William Reay, Kuraray, FVAL Division

It may have two zones, in which compression takes place in the first zone and homogenizing in the second zone. Most often there are three zones: transport, compression, and homogenizing zones. The pitch is constant throughout, but the shaft diameter is low in the first zone and increases gradually to a highest value in the second zone. In the third zone it is once more constant. The compression zone may be short with high gradient, which is suitable for thermally robust resins like PE or PP, or it may be a bit long for thermally sensitive resins. Screws may have a decompression zone with a higher channel depth just after the compression zone. This enables the gas bubbles, which arise particularly when working with recycled resins, to move up and leave the extruder through a valve. In some high-quality screws there is a shearing part, for example, a Maddock element. The diameter of the screw shaft is highest in this part so that the melt has the narrowest possible route through the extruder. This causes the specks to press against the barrel inner wall and ultimately melt.

Finally, there may two different types of barrier screws. The barrier screws have a transition flight after the compression and shearing parts. The objective of the transition flight is to separate the specks from the melt, press them into this part, and ultimately melt them completely. There are two types of barrier screws. One is named after Maillefer, this one having a variable pitch for the transition flight but constant shaft diameter, and the other after Barr, this one with variable channel depth but constant pitch for the transition flight.

### **Types of Barrels**

There are two types of barrels: a barrel with a constant inner diameter and a barrel that has a number of slant grooves in the feed zone. The grooves are placed symmetrically along the perimeter of the barrel with the highest depth at the beginning, which reduces gradually and vanishes after some 3 to 4 D with the inner diameter of the barrel. Through the first type of barrel, a constant amount of resin can always be processed. In a three-zone extruder with such a barrel, the highest melt pressure, around 200 bar, is always at the end of the compression zone.

In a grooved barrel, in contrast, more resin can be transported at the beginning through the grooves than in a normal barrel, and the highest pressure of the melt is just after the position where the grooves end. The highest melt pressure in a grooved barrel is around 1000 bar and is much higher than in a nongrooved one. It is therefore easier to furnish a screw with different parts like shearing or barrier parts, which need more power to drive. Not all types of resin are suitable to be extruded in a grooved cylinder. Resin suppliers advise the manufacturers whether it is suitable for a grooved feed zone or not.

### **Universal Extruder**

A universal extruder is a machine where different resins may be processed. It has no barrier part and only sometimes a shearing part. It is suitable to produce an acceptable quality of melt with different resins. The extruder is optimized for a broad spectrum of applications, such as LDPE, HDPE, LLDPE, EVA, and ionomers with different additives.

### **High-Performance Extruder**

A high-performance extruder is one that has to produce a very high quality melt out of resins to produce a high-quality product. The extruder screw is specially constructed to match a particular polymer like nylon (PA), PET, or PS. Other types of polymers or even resins with some additives cannot be worked with these extruders at sufficiently high quality. The objective of a high-performance extruder is to produce very high quality product, mostly films for a particular application. High-performance extruders always have a shear part, if not barrier parts.

### Coextrusion

Packaging performance can, in most cases, not be fulfilled by a single layer of material. Properties of different resins or other packaging materials like paper or aluminum are combined into a multilayer packaging material called a composite. These are the ideal packaging material to fulfill different requirements.

Different layers of composites are written in a line with a slash between the layers, like PET/Al/PE 12/8/60, or the layers can be written one on top of another, like below.

PET 12 Al 8 PE 60

The first version takes less space and is easier to write. The layer thicknesses are written next to the composite in micrometers ( $\mu$ m). In this book the first version will be used. The left side represents the outer layer and the right side the inner

layer. The inner layer has most of the sealing function: it is in direct contact with the product, for example, food. This layer must fulfill all of the legislative requirements. For a pure polymer composite, all of the resins of the different layers are melted in different extruders, and the melts are combined in a suitable series to make the final packaging material (Fig. 2.3).

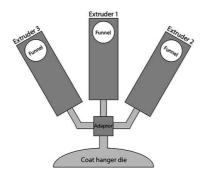


Figure 2.3 Coextrusion line with three extruders

Because the bonding forces between the layers of most resins are not high enough, special bonding resins are necessary, which are called tie resins. For each type of resin, main layer, or tie layer, one extruder is necessary. The suitable layer structure is built in a feed block, where the different melt streams from the extruders are fed. The feed block is the heart of a coextrusion line (Fig. 2.4).



Figure 2.4 Coextrusion with three extruders, feed block, and coat hanger die, courtesy of Battenfeld

# Index

acetaldehyde 14 acrylic 97 additives 5 adhesive 89, 92 air knife 32 Al<sub>2</sub>O<sub>3</sub> 100 Al barrier laminate 37 AlOx 100 aluminum 36 amine light stabilizer XVI amorphous XVII, 3 antiblock 6 antifog agents 6 antimicrobial 8 antioxidants 5 antistatic 7 aromatic 5 aseptic 69 atactic 13 auger dosing 109

### В

bags 12 barrel 19 barrier 22, 25 biaxial-oriented XV blends 5 blocking 30 blowing agents 8 blown film 27 blow-up ratio 28

BOPA / BONy) XV bottles 12,14 boxes 77 branching 3 brittle 4 bubble 26

### С

calendering 33 caps 49 cast films 46 cast sheets 33 catalysts 5 cavity 49 ceramic barrier laminate 37 channels 44 chemical resistance (ESCR) 8 chemical vapor deposition chill roll 31 clarity 16 closure 39 coat hanger die 21

coating 84 coefficient of friction 6 coextrusion 84 COF XV cohesion 85 coinjection 51

collapsible tube 112 colorants 7 composite cans 98 composites 79 compounding 4 compression 19 condensation 102 conduction 63, 73 converting 83 copolymers 90 core 28 corona treatment 30, 85 cosmetics VII, 107 covalent bonds 29 CPP 88 craters 112 cross-linking 93 crystalline 3 crystallites 3 Curing 85 curtain 102

deformation 4 degradation 5 density 9 deposition 14 die 24 die-cut lid 70 dielectric 77 diffusion 29

fillers 65

film 89

filter 88

dimensional stability 46 flexible 90, 100 hydrogen bonding 2 dispersion 84,85 - packaging 13 double-bubble 42 flow 26 fluoroelastomers 48 drape forming 70 dry lamination 84 fluoropolymers 48 impact 110 duroplastics 4 foam extrusion 106 induction sealing 74 infrared XVI, 88 foaming 84 foam injection molding injection blow molding Ε 106 53 EAA 11 foam thermoforming 107 injection molding 50 elastic 46 fog 6 in-line thermoforming 68 foil 11, 37 elasticity 61 in-mold labeling (IML) 55 inner sealing layer 30 elastomer 104 food packaging 42, 44 electron beam gun 101 friction 73 ionomer 40, 73 frost line 27 electrostatic 39 isotactic 13 elongation 60 functional layers 55 isotropic 46 environmental stress funnel 21 crack resistance (ESCR) Κ 83, 111 G epoxy phenol 36 kaolin 67 EPS XVI gamma radiation 104 erucamide 7 gas flame 29 L ESCR 83, 111 gelation 88 ethylene-acrylic acid coglass transition temperalabel 15 polymer 11 ture 61 lacquers 29 lamination 37, 84 ethylene-butyl acrylate glue 97 copolymer 11 glycol XVII lap seal 37 green tack 85 ethylene-methacrylic acid latex 88 grooves 22 LDPE XVI leakage 37, 70 ethylene-vinyl acetate 11 EVOH 14, 15 lips 31 LLDPE XVI extruder 17 extrusion 19 HALS XVI longitudinal sealing 35 extrusion blow molding HCI XVI lubricants 6 54 HDPE XVI HDT XVI М head 4 F heat seal lacquer 87 machine 6 fatty acid 5 HFFS 109 macromolecules 1,12 feed block 24 HIPS XVI magnetic 79 hot air 42 male (positive mold) 65 female (cavity) 65

hot fillable 16

hot knife 54

hot melt 85

hot tack 10, 13

mandrel 38

masterbatch 5

MAP 40

MDPE 9

medical 14
melt flow 6, 51
melting point 61
melt temperature 51, 61
metallocene XVI
metering zone 20
migration 25
mixing 34
mLLDPE XVI
modulus 61
moisture 83
molding 54
molecular weight 61
monomers 93
MXD6 XVI

## Ν

NaOH 13 neck-in 31 needle closures 51 negative forming 65 nip rolls 27, 86 nonpolar 77 nucleating agents 106

### 0

oleamide 7 opaque 7 OPLA XVI OPS XVI orientation 3, 42 oxidation 102 ozone 29

### Ρ

PA XVI PAN XVI paneling 81 parison 55 peel sealing 72 permeation 113 PET XVII

PET-A XVII PET-C XVII PET-G XVII pharmaceutical blisters 15 phenols 5 phosphites 5 phthalates 15 pigments 55 pinhole 100 plasma 101 plasticized polyvinyl chloride XVII plasticizers 11 plastomers 80 plug assistance 61 polarized 80 polyaddition 1

polyamide / nylon XVI
polycondensation 1, 60
polyester 10
polyethylene VII
polyethylene naphthalate
XVII
polyethylene terephthalate
XVII
polylactic acid XVII

polymer barrier laminate 37
polymerization 1
polyolefin XVII
polystyrene XVII
polytetrafluoroethylene XVII
polytetramethylene terephthalate XVII
polyurethane 2
polyvinylchloride 3
positive forming 65

preforms 14 prepolymers 85 pressure 86 primer 86 processing aids 6

pot life 85

propagation 94 properties 48 PVC-P 105 PVD XVII PVdC XVII PVOH XVII

## α

quartz 64

### R

radiation 64
radiation upgrading 104
radicals 104
reactive 103
recycling 28
regulations 41
relaxation 44
responsibility of a
producer 9
retention force 111
retorting 46
roll stocks 41
RPM 21
rubber 75

### S

sachets 109
sacks 12
scrap 25
screw 22, 25
sealing 24, 26
- integrity 72
- jaw 72
- layer 72
- pressure 72
- strength 72
- through dust 80
- through liquid 80
- time 72
semicrystalline 3

shearing 22

sheet 25 shelf life 40 shrink films 41 shrinking 42 side-folded pouches 109 silicon dioxide XVII silicon monoxide XVII single screw extruder 5 SiOx XVII skin packaging 70 sleeves 45 slip agent 5 solid content 94 solvent based 87 solvent-free 87, 93 specific heat 102 spectrum 5 spherulites 3 SPPF (solid phase pressure forming) 61 squeezing 35 stabilizer 5 stiffness 5 strain 74 strength 74 stress crack 111 stretch 14 stretch blow molding 56 surface tension 29 swelling 106 syndiotactic 13

TiO<sub>2</sub> 62 tools 21 toughness 16 transparency 28 transverse direction 42 transverse sealing 72 triple-bubble 44 tubes 49 twin screw extruder 4

### IJ

ultra low density PE 11 unplasticized polyvinyl chloride XVII unsaturated 1 UV 39, 41

### ٧

vacuum deposition 83
vacuum-shrink pouches
41
van der Waals forces 2
very low density PE 11
VFFS (vertical-form-fillseal) 72, 109
vinylacetate 9
viscosity 20
volumetric dosing 109

### W

tandem 105
tearing 40
tensile 40
tentering 47
thermoform-fill-seal (TFFS)
65, 68
thermoforming 48
thermoforming window 61
thermoset plastics 4
tie layer 13, 24
tightness 37

T

waste 49
water bath 42
water bath sheets 33
wavelength 64
wet lamination 84
winding 94
wrapping 97

Υ

yield 73